## Amendments to the Claims

This listing of claims will replace all prior versions, and listings, of claims in the application:

## Listing of Claims:

(Currently amended) A method of producing polyethylene, the method comprising:
 combining ethylene and at least one α-olefin selected from C<sub>3</sub> to C<sub>10</sub> α-olefins, an
 activator, and a metallocene catalyst compound to produce a polyethylene;
 wherein the metallocene catalyst compound is selected from:

$$R^{10}$$
 $R^{9}$ 
 $R^{1}$ 
 $R^{2}$ 
 $R^{3}$ 
 $R^{4}$ 
 $R^{4}$ 
 $R^{5}$ 

wherein M is a Group 4 atom; X is a leaving group; n is an integer from 0 to 3; and

R<sup>1</sup> to R<sup>12</sup> are independently selected from the group consisting of hydrides, halogens, hydroxy, C<sub>1</sub> to C<sub>6</sub> alkoxys, C<sub>1</sub> to C<sub>6</sub> alkenyls, and C<sub>1</sub> to C<sub>10</sub> alkyls, provided that the tetrahydroindenyl is substituted; and

characterized in that when the comonomer is 1-hexene, and the mole ratio of 1-hexene to ethylene combined is varied between 0.015 to 0.05, the density of the resultant polyethylene changes by less than 5 % and the I<sub>21</sub>/I<sub>2</sub> varies from 10 to 150.

2. (Original) The method of Claim 1, further characterized in that the  $I_{21}/I_2$  of the polyethylene varies from 15 to 100.

- 3. (Original) The method of Claim 1, wherein R<sup>1</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>10</sub> alkyls.
- 4. (Original) The method of Claim 1, wherein R<sup>1</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>5</sub> alkyls.
- 5. (Original) The method of Claim 1, wherein R<sup>1</sup> to R<sup>4</sup> and R<sup>7</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>10</sub> alkyls, and R<sup>5</sup>, R<sup>5</sup>, R<sup>6</sup>, and R<sup>6</sup> groups are hydride.
- 6. (Original) The method of Claim 1, wherein the combining takes place under gas-phase polymerization conditions.
- 7. (Original) The method of Claim 1, characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05, the density of the resultant polyethylene changes by from less than 2 %.
- 8. (Original) The method of Claim 1, further characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05 the amount of methyl groups per 1000 carbon atoms of the polyethylene produced therein is from less than 20.
- 9. (Original) The method of Claim 1, further characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05 the amount of comonomer incorporated into the polyethylene produced therein ranges from less than 12 wt% of the total weight of the polyethylene.
- 10. (Original) The method of Claim 1, wherein the activator and metallocene catalyst compound are supported on a carrier material.

- 11. (Original) A polyethylene produced by the method of any one of Claims 1 through 10 having an I<sub>21</sub>/I<sub>2</sub> value of from 10 to 300, an M<sub>w</sub>/M<sub>n</sub> of 1.9 to 6, and a density of from 0.88 to 0.97 g/cm<sup>3</sup>.
- 12. (Currently amended) A catalyst system comprising: an activator and a metallocene catalyst compound; wherein the metallocene catalyst compound is selected from:

$$R^{10}$$
 $R^{9}$ 
 $R^{1}$ 
 $R^{2}$ 
 $R^{3}$ 
 $R^{4}$ 
 $R^{4}$ 
 $R^{4}$ 
 $R^{5}$ 

wherein M is a Group 4 atom; X is a leaving group; n is an integer from 0 to 3; and

- R<sup>1</sup> to R<sup>12</sup> are independently selected from hydrides, halogens, hydroxy, C<sub>1</sub> to C<sub>6</sub> alkoxys, C<sub>1</sub> to C<sub>6</sub> alkenyls, and C<sub>1</sub> to C<sub>10</sub> alkyls, provided that the tetrahydroindenyl is substituted; and
- characterized in that when one or more metallocenes and an activator are combined with ethylene and 1-hexene, and the mole ratio of 1-hexene to ethylene combined is varied between 0.015 to 0.05, the density of the resultant polyethylene changes by less than 5 % and the I<sub>21</sub>/I<sub>2</sub> varies from 10 to 150.
- 13. (Original) The catalyst system of Claim 12, further characterized in that the  $I_{21}/I_2$  of the polyethylene varies from 15 to 100.
- 14. (Original) The catalyst system of Claim 12, wherein R<sup>1</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>10</sub> alkyls.

- 15. (Original) The catalyst system of Claim 12, wherein R<sup>1</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>5</sub> alkyls.
- 16. (Original) The catalyst system of Claim 12, wherein R<sup>1</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>3</sub> linear alkyls.
- 17. (Original) The catalyst system of Claim 12, wherein R<sup>1</sup> to R<sup>4</sup> and R<sup>7</sup> to R<sup>12</sup> are groups selected from the group consisting of hydride and C<sub>1</sub> to C<sub>10</sub> alkyls, and R<sup>5</sup>, R<sup>5</sup>, R<sup>6</sup>, and R<sup>6</sup> groups are hydride.
- 18. (Original) The catalyst system of Claim 12, wherein the density of the resultant polyethylene changes by less than 2 %.
- 19. (Original) The catalyst system of Claim 12, further comprising a carrier, wherein the activator and metallocene catalyst compound are supported on the carrier.
- 20. (Original) The catalyst system of Claim 12, characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05, the density of the resultant polyethylene changes by from less than 2 %.
- 21. (Original) The catalyst system of Claim 12, further characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05 the amount of methyl groups per 1000 carbon atoms of the polyethylene produced therein is from less than 20.
- 22. (Original) The catalyst system of Claim 12, further characterized in that when the mole ratio of 1-hexene to ethylene combined is varied from 0.02 to 0.05 the amount of comonomer incorporated into the polyethylene produced therein ranges from less than 12 wt% of the total weight of the polyethylene.